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Research

Determining the Pulping Conditions and Properties of Unbleached Pulp from Uruguayan *Pinus Taeda*

Determinación de las condiciones de pulpeo y propiedades de pulpa marrón a partir de *Pinus taeda* Uruguayo

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Abstract

Context: In Uruguay, numerous *Pinus taeda* plantations are at final-turn age, but they still do not have commercial destination and are exported as green-wood logs. For the development of this sector, it is necessary to strive towards a comprehensive processing of this resource.

Method: This work focused on analyzing the use of *Pinus taeda* wood available in the country to produce brown kraft pulp with a kappa number of 80, which can be used to make packaging paper. As raw materials, we employed by-products from the mechanical wood-transformation industry (wood chips and thinning wood) and final-turn wood. Pulping tests were carried out, varying the alkali charge and the H-factor while aiming for a kappa number of 80. The viscosity, pulping, and rejection yield were measured in the pulps, and the pH and residual alkali content were evaluated in black liquor.

Results: Based on the results, the best pulping conditions were an active alkali charge of 14% (Na_2O) and an H-factor of 1260 for sawmill chips and thinning wood, as well as an active alkali charge of 14% (Na_2O) and an H-factor of 1080 for final-turn wood. The pulp obtained with sawmill chips exhibited the most resistant fibers, and the final-turn wood pulp was the most sensitive to the refining process. Under the aforementioned conditions, the paper properties of laboratory-produced pulp are comparable with those of commercial pulp.

Conclusions: This indicates that it is technologically possible to produce brown kraft pulp from Uruguayan *Pinus taeda* wood, with adequate quality to produce packaging paper.

Keywords: kraft pulp, *Pinus taeda*, paper properties

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Resumen

Contexto: En Uruguay existen numerosas plantaciones de *Pinus taeda* que están en edad de turno final, pero que aún no tienen un destino comercial y se exportan como troncos verdes. Para el desarrollo de este sector, es necesario buscar un procesamiento integral de este recurso.

Método: Este trabajo se enfocó en analizar el uso de la madera de *Pinus taeda* disponible en el país en la producción de pulpa *kraft* marrón con un número *kappa* de 80, que puede utilizarse para fabricar papel de embalaje. Como materia prima, se emplearon subproductos de la industria del aserrado (*chips* y madera de raleo) y madera de turno final. Se realizaron ensayos de pulpeo, variando la carga de álcali y el factor H con el objetivo de alcanzar un número *kappa* de 80. Sobre las pulpas se midieron la viscosidad, el rendimiento del pulpeo y el rechazo, y se evaluaron el pH y el contenido de álcali residual sobre el licor negro.

Resultados: Con base en los resultados, las mejores condiciones de pulpeo fueron una carga de álcali activo del 14 % (Na_2O) y un factor H de 1260 para los *chips* de aserradero y la madera de raleo, así como una carga de álcali activo del 14 % (Na_2O) y un factor H de 1080 para la madera de turno final. La pulpa obtenida con *chips* de aserradero presentó las fibras más resistentes, y la pulpa de madera de turno final fue la más sensible al proceso de refinado. Bajo las condiciones mencionadas, las propiedades papeleras de la pulpa producida en laboratorio son comparables con las de la pulpa comercial.

Conclusiones: Esto indica que es tecnológicamente posible producir pulpa *kraft* marrón a partir de madera de *Pinus taeda* uruguaya, con la calidad adecuada para producir papel de embalaje.

Palabras clave: pulpa *kraft*, propiedades papeleras, *Pinus taeda*

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1. Introduction

In Uruguay, the forest industry has been bolstered since the approval of the second Forest Law in 1987, increasing the area of forest plantations from 80 000 ha in 1988 to more than 1 000 000 in 2018 (1). Since 2007, the production of bleached kraft pulp from eucalyptus wood has positioned itself as one of the leading markets in the country. However, the processing of pine wood is focused on the production of sawn boards and plywood in small and medium-sized production plants and in a context where wood supply widely exceeds the demand, resulting in the accumulation of this raw material (1, 2). Likewise, the production yields are approximately 50 %, generating 1 000 000 m³ of chips and cutouts on an annual basis. In addition to the accumulation of final-turn wood, 1 400 000 m³ of thinning wood are produced annually and are underutilized (3). Currently, this biomass is used for power generation, but, due to changes in the country's energy matrix, including the installation of wind farms and the energy input from eucalyptus kraft pulp production mills, this alternative will not be economically sustainable in the future (4).

On the other hand, the consumption of packaging paper is increasing worldwide, with a compound annual growth rate (CAGR) of 2.3 % in 2021 (5). This is due to increases in international trade and human consumption. The rise in trade implies a greater consumption of packaging paper (6) and, consequently, an increase in the consumption of brown pulp, with the growth forecast being 4.6 % by 2030 (7). Additionally, there is a trend towards replacing non-removable plastic packaging with packaging made from more sustainable materials like paper.

Kraft cooking is the most used pulping method worldwide due to several advantages: the good quality of the pulp produced, the fact that the recovery cycle allows operating with low replacement and on large production scales, and its low environmental impact in modern mills (6,8). This method focuses on dissolving lignin while preserving the highest possible fraction of cellulose and hemicellulose in the pulp. Since the objective of this work is to obtain unbleached pulp, a greater portion of lignin and hemicellulose remains in the pulp, which increases the cooking yield and improves the properties of the paper (8,9).

The main operating parameters in the kraft process are the alkali charge and the H factor. The first indicates the amount of sodium hydroxide and sodium sulfide that is added to the digester per ton of wood, and the second is a combination of time and the temperature at which the process is carried out, according to Arrhenius-type kinetics, in order to reach a predetermined value regarding the *kappa* number of the pulp at the digester discharge (9). For pine wood used in the production of packaging paper, the alkali charge typically varies between 15 and 20 % (as Na₂O), and the H factor is between 750 and 2040 (10–15).

In kraft cooking, sodium hydroxide and sodium sulfide are used as active chemicals. Sodium hydroxide provides the alkaline medium for lignin solubilization, while sodium sulfide degrades lignin and makes the process more selective, as fewer amounts of hemicelluloses are solubilized. It is worth adding that the wood is chipped prior to being fed to the digester, so the shape and size of the chips

determine the vaporization and impregnation performance, as well as the heat and mass transfer in the digester (8,16). The feasibility of using wood that was chipped for another purpose (chip subproducts of sawn wood) should be evaluated.

Paper properties are a set of physical, chemical, and physicochemical measurements that allow characterizing a sample of paper or cardboard. To carry out these measurements, the pulp sample is subjected to a refining process, and manual sheets are subsequently formed. The refining extension must be enough to produce fibrillation of the fibers in order to enable sheet formation, but it cannot be excessive to the point of damaging the integrity of the fibers (17).

The degree of refinement is quantified by determining drainability, which measures the interaction between fibers in forming a framework. This measurement is carried out using the Canadian Standard Freeness (CFS) method. In the industrial production of packaging paper, elongation properties are the most relevant, especially tensile strength, which depends on the length of the fibers and the links between them, and the bursting resistance, which evaluates the overall paper strength. Tear resistance is also measured as a strength property. To characterize paper, grammage, thickness, air permeability, and opacity are also usually determined (11,18).

The aim of this work was to evaluate the quality of the available *Pinus taeda* wood in Uruguay to produce unbleached kraft pulp, determining the pulping conditions for residues from mechanical wood processing, thinning, and final-turn wood. In addition, selected pulping conditions were used to evaluate the paper properties of the selected pulps, aiming to establish whether it is technologically possible to market them as inputs for the production of packaging paper.

2. Materials and methods

2.1. Raw materials

Pinus taeda chips were provided by a sawmill located in the department of Rivera (Uruguay), using 24-year-old clearcut logs with an average diameter at the fine point of 40 cm. We also tested 20-year-old final-turn clearcut *Pinus taeda* logs with apical diameters of 54.3, 40.0, and 38.6 cm from the department of Tacuarembó (Uruguay), as well as 16-year-old wood from commercial thinning, with apical diameters of 28.2, 30.9, and 22.0 cm, also from the department of Rivera. In the last two cases, the material was chipped, and a mixture composed of three specimens and six branches was produced.

To compare the papermaking properties of this wood against available commercial samples, two samples of brown kraft pulp from *Pinus radiata* were used.

2.2. Drying and classification

The chips of the three types of wood were processed separately. First, they were classified in a tray sieve (Regmed 87 model CC-2, Technical Industry of Precisao Ltda., Brazil) according to the SCAN-CM 40:01 standard.

The 'accepted chips' were dried in a Nardi tray dryer with induced draft air circulation (12 Hz) at 40 °C for 72 h, reaching a final humidity of 8 %. They were kept in a dry environment and not exposed to solar radiation until use.

2.3. Physicochemical characterization of the wood

The basic density was determined using the TAPPI T 258 OM-16 standard. The extractives were quantified using water and ethanol as solvents (19). The extractive-free biomass was characterized in terms of carbohydrates, aliphatic acids, and acid-soluble and -insoluble lignin according to the National Renewable Energy Laboratory's procedure (NREL) (20), using an HPLC instrument (Shimadzu Corporation, model LC20, Kyoto, Japan) with a refractive index and UV-visible detectors. With regard to the aforementioned procedure, it is worth noting that only the Aminex HDX-87H column was used, with a flow of 0.6 mL/min, a temperature of 45 °C, and 0.005 M of sulfuric acid as the mobile phase. Soluble lignin levels were measured by spectrophotometry (Shimadzu Corporation, model UVmini-1240) at a wavelength of 240 nm, considering an absorptivity of 12 L/g.cm according to the NREL procedure (20). The ash content was determined by following the TAPPI T 211 standard.

2.4. Brown kraft pulp production

Pulping tests were carried out on the chips obtained from the sawmill. Once the best conditions for these chips were established, tests were carried out in limited condition ranges on the chips from thinning and final-turn wood.

A thermostatic oil bath with eight 316 stainless steel rotating cylinder vessels was used for pulping. Each vessel had a volume of 300 mL (Fibretec model FBI PT 2002B, India). The maximum cooking temperature was fixed at 170 °C, the wood liquor ratio was 4.5:1, and the percentage of sulfidity was 30 %. The alkali charge varied between 14 % and 19.5 % (Na₂O), which was determined by following the ISO AWI 23774 standard, and the H-factor was set at 720, 900, 1080, or 1260. The H-factor is a process control variable that expresses the cooking time and temperature in batch reactors as a single variable. Geometrically, it is the area under the relative rate of reaction *vs.* the time curve (8).

After cooking, the pulp was washed by hand in cloth bags. In the first instance, it was washed using three spin cycles, and a total 2 L of deionized water were used per cycle. After the last cycle, the cloth bag with the pulp remained submerged in deionized water for 24 h. After that time, a fourth washing cycle was conducted, and the pulp was stored at 4 °C until analysis.

The pulp was refined using a disc refiner (Kumagai Riki Kogyo Co., Ltd., Tokyo, Japan) until the defibrillation point was reached. This value was determined by observation under a microscope. The refiner disks were 30 cm diameter, and the gap between them was 1.12 mm.

The refined pulp was homogenized at 2000 rpm (Kumagai Riki Kogyo Co., Ltd., Tokyo, Japan) and sorted using a separating sieve (Kumagai Riki Kogyo Co., Ltd., Tokyo, Japan) with a 0.15- mm slotted plate for 20 min and under 8 kg/cm² of water pressure.

2.5. Black liquor characterization

For the black liquor obtained after cooking, the final pH and residual alkali were determined according to the ISO AWI 23775 standard.

2.6. Pulp characterization

The pulp water content was determined by drying at 105 °C, as per the ISO 638 standard. We also calculated the cooking yield was, defined as the relation between the mass of the dry pulp obtained and the mass of the dry chips fed to the reactor. The percentage of rejected pulp was determined, defined in turn as the mass of dry rejects retained in the separating sieve in relation to the total dry pulp mass.

For the accepted pulp, the *kappa* number (ISO 302) and the viscosity (ISO 5351) were determined. The standard for viscosity determination applies to pulps with low lignin content (less than 5%); otherwise, dissolution in cupriethylene diamine is not completed. In order to use this standard, the literature proposes dissolution, followed by filtering the material before carrying out the measurement measuring (21).

2.7. Disaggregation of commercial pulps

Commercial samples were received in sheets with 90 % dryness. These samples were separated into 2 cm² pieces and left in distilled water for 24 h at room temperature, with a ratio of 24 g of dry pulp per L of water. The hydrated pieces were disintegrated with 2 L distilled water at 40 °C in a disintegrator pulper (Universal Engineering Corporation, model UEC-2008, India) for 15 min.

2.8. Paper properties

The pulp was refined at 6000, 9000, and 12 000 revolutions in a PFI mill (model no. 209, Hamjern, Oslo, Norway; TAPPI Test Method T 248 sp15, 2015). The drainability was determined by measuring the Canadian Standard Freeness (CSF), following the TAPPI T 227 om-17 standard. Ten manual sheets were formed per sample, according to the ISO 5264-2 and ISO 5269-2 standards, and conditioned at 23 °C and 50 % humidity for at least 4 h according to the ISO 536.

The sheets were used to determine grammage, thickness, opacity, and air permeability, as per ISO 536, ISO 534, ISO 2471, and ISO 5636-5, respectively. As for the mechanical properties, tensile strength, tear resistance, and burst strength were determined by following TAPPI T 494 om-01, ISO 1974, and ISO 2758.

The resistance indices were calculated as the relationship between the resistance and the average weight of the sample at a given degree of refinement.

2.9. Calculation of uncertainties and statistical analysis

The statistical error for the structural components of the biomass was calculated as twice the standard deviation. The error for the H-factor corresponds to the contribution during ± 1 min at maximum temperature. The error in alkali loading and residual alkali corresponds to ± 0.1 mL of titrant during titration. The errors of the other parameters were calculated according to the recommendations of their corresponding standard methods. To compare the paper properties, the reported error was taken as the standard deviation. Regarding statistical treatment, an ANOVA was performed while using Tukey's test with a confidence value of 95 %. The tables corresponding to the paper properties present an analysis that considers each sample and the number of revolutions as partitions (lowercase and uppercase, respectively).

3. Results and discussion

3.1. Chemical characterization

85 % of the sawmill by-product chips had a suitable size for use in the kraft pulping process, whereas 11 % were larger and could be re-chipped.

The sawmill chips exhibited a basic density of 466 ± 2 kg/m³, while the final-turn wood reported 442 ± 10 kg/m³ and thinning wood showed 432 ± 6 kg/m³. These values are within the range reported in the literature for *Pinus taeda* wood (10,22). The thinning and final-turn wood samples exhibited lower basic density values, which may be due to the fact that the samples contained branches. Branches have higher lignin content because of the reaction wood that is generated during their growth. Lignin is a hydrophobic compound, so, for the same mass of dry solid, the volume saturated in water is lower.

Table I shows the chemical composition of the three types of wood, expressed as grams per 100 grams of dry wood. Carbohydrates (cellulose and hemicelluloses) are presented as their constituent monomers. The contents of xylose, mannose, and galactose are expressed as xylose equivalents, as the chromatographic column used does not allow separating these three monomers.

The three types of wood exhibited similar carbohydrate content (glucose, arabinose, xylose, mannose, and galactose). However, the sawmill chips had lower extractives and lignin contents, favoring the pulping process. The higher content of lignin and extractives in the thinning and final-turn wood could be explained by the presence of branches in the composition of the starting mixture, as mentioned above.

3.2. Sawmill chips

As previously mentioned, the selection criteria for pulping were adjusted using sawmill chips and performing kraft pulping under the conditions mentioned in section 2.4. Once the best conditions were found, a narrow search of conditions was performed for the thinning and final-turn wood.

Table I. Chemical characterization of the different *Pinus taeda* woods used in this work

	Sawmill chip	Thinning wood	Final-turn wood
Ash	0.37±0.02	0.35±0.02	0.33±0.02
Extractives in water	1.56±0.38	2.16±0.10	3.08±0.32
Extractives in ethanol	1.90±0.08	3.39±0.04	2.27±0.08
Insoluble lignin	27.9±1.4	29.7±2.6	28.8±0.8
Soluble lignin	3.1±0.6	4.1±1.2	4.8±2.4
Glucose	47.2±4.2	45.4±1.0	47.2±3.6
Arabinose	2.8±1.5	2.9±0.6	2.3±0.3
Xylose+mannose+ galactose (as xylose)	9.4±0.5	9.8±0.3	9.5±0.3

3.2.1. Kraft pulping

Table II shows the results obtained for the different pulping conditions of the sawmill chips.

Table II. Properties of the pulps obtained after applying different conditions to the sawmill wood chips

Test number	H factor (±17)	Alkali charge (%Na ₂ O) (±0.5)	Yield (%)	Kappa number	Rejects (%)	Viscosity (mL/g)
1	733	13.4	67.1±2.0	117.5±5.8	5.3	209±16
2	721	17.1	54.6±1.4	112.9±8.0	5.3	319±14
3	733	19.5	48.1±1.6	62.5±3.8	2.5	659±12
4	973	16.5	53.0±1.8	101.6±0.8	1.3	413±14
5	909	18.7	53.3±2.0	82.0±3.0	3.0	520±22
6	1,092	12.9	58.1±1.6	115.2±0.8	3.7	348±12
7	1,077	16.0	60.7±1.2	85.1±5.8	1.1	626±14
8	1,082	17.1	56.0±3.4	76.6±0.6	4.6	789±14
9	1,084	19.1	46.2±1.2	61.2±0.2	0.7	957±6
10	1,268	14.0	52.5±1.4	83.7±1.2	0.3	741±8
11	1,266	14.5	51.1±4.2	78.0±1.4	1.2	1,018±6
12	1,26	15.0	52.9±1.4	67.8±1.0	0.5	869±12
13	1,265	16.1	41.4±1.4	52.6±2.4	0.1	1,284±10
14	1,258	16.8	44.7±1.8	45.5±2.4	0.4	1,199±12

The yield values obtained (50-65% for a *kappa* number greater than 68 and 40-50% for a *kappa* number of less than 68) are similar to those reported in the literature and are consistent with the

characteristics of the process (10–15). Note that, the higher the degree of delignification, the lower the residual lignin content – thus, a lower *kappa* number can be obtained. This also entails a greater loss of carbohydrates, which further contributes to the decrease in yield. If the variation of the *kappa* number is analyzed within the same H-factor range, the expected trend is obtained. This is because, when the alkaline load decreases, the *kappa* number and the yield increase.

The percentage of rejection for the samples with a *kappa* number between 70 and 80 was within the expected range (0.9-6.9%). However, the tests with more severe pulping conditions reported a lower rejection percentage, corresponding to a higher degree of delignification (which can be seen as a lower *kappa* number). Nevertheless, there were samples (such as number 10) that deviated from the general trend. It is worth stating that a greater delignification decreases the rigidity of the matrix, which makes the mechanical refining stage more effective, resulting in a lower number of fiber bundles retained in the screening stage.

In the viscosity analysis, the expected trend was not found, since the increment in the alkali load produced greater carbohydrate degradation and a decrease in the degree of polymerization. However, the viscosity value increased. This could be explained by the experimental procedure used; due to the high lignin content, the tested samples did not completely dissolve in the cupriethylene diamine. In the samples with lower lignin contents (*i.e.*, a lower *kappa* number), the dissolved material in the cupriethylene diamine was higher, since cellulose was more available. Consequently, the viscosity value increased. Therefore, only samples with similar *kappa* numbers should be compared. In these cases, the viscosity value increased when the alkali load decreased, and the H-factor increased, which was the expected trend. It can be concluded that, for samples with a similar *kappa* number, those that were produced with a lower alkali load exhibited a higher viscosity (8,21).

Considering the results reported in Table II, tests 7 (H-factor: 1077; alkali load: 16.0% Na₂O) and 10 (H-factor: 1268; alkali load 14.0% Na₂O) were selected as the best conditions, given that, out of the samples with a *kappa* number in the range of 80, they reported the highest yields and viscosity values, as well as a lower rejection content.

3.2.2. Black liquor

In all the tests carried out, the final pH of the black liquor showed values greater than 11. Thus, there was no risk of lignin precipitation. The samples that reported values of residual active alkali (RA) within the recommended range (2-4 g/L as Na₂O) were numbers 6, 7, and 11. Considering the RA recommended by the literature and the volume used in each test, the recommended value was 0.48 to 0.96 g as Na₂O. The samples with an RA of less than 0.96 g as Na₂O exhibited a higher degree of polymerization, and, consequently, they yielded pulp of better quality (8).

3.2.3. Thinning and final-turn wood

The thinning and final-turn wood samples were analyzed using test 10, which was selected because it demonstrated the lowest active alkali consumption among the two best conditions. Under these

conditions, a $kappa$ number of 72.0 ± 0.9 was reached with the final-turn wood. In order to reach the target $kappa$ number of 80, the same active alkali charge was used, and the H-factor decreased (H-factor: 1077; alkali load: 14 % as Na_2O). This could be explained by the presence of compression wood in the sample composition (23).

Table III shows the results for the thinning and final-turn wood, as well as for the sawmill chips obtained with the same active alkali load and the highest H-factor.

Table III. Results for the kraft pulping of thinning and final-turn wood when compared to sawmill chip wood under similar pulping conditions

	Alkali charge (% Na_2O)	H factor	Kappa number	Yield (%)	Rejection (%)	Viscosity (mL/g)
Final-turn wood	14.0 ± 0.5	$1,077 \pm 17$	79.0 ± 2.0	48.9 ± 1.2	0.3	938 ± 14
Thinning wood	14.0 ± 0.5	$1,268 \pm 17$	80.0 ± 2.4	50.7 ± 2.8	0.9	874 ± 6
Sawmill chip wood	14.0 ± 0.5	$1,268 \pm 17$	83.7 ± 1.2	52.5 ± 1.4	0.3	741 ± 8

The pulping yields, using 14 % active alkali (Na_2O), were similar for the three types of wood. Likewise, in all cases, the percentage of rejection was within the expected range, as reported by other authors (24, 25).

On the other hand, the viscosity values of the pulps obtained from thinning and final-turn wood were higher than those from sawmill chips. In the case of the final-turn wood, the high viscosity was likely due to the lower H-factor used, which implies less severe cooking conditions and, therefore, less attacking of the cellulose chains. As for the thinning wood, a higher rejection value was obtained. Thus, more severe conditions would be needed to match the degree of cooking of the sawmill chip wood. The thinning wood's lower degree of cooking was also reflected in a higher viscosity value.

3.2.4. Commercial pulp samples

The commercial samples, called *commercial sample 1* (CS1) and *commercial sample 2* (CS2), exhibited relatively low $kappa$ numbers (CS1: 33 ± 3 and CS2: 40 ± 4 , respectively). In addition, comparable viscosity values were obtained (973 ± 4 mL/g for CS1 and 882 ± 4 mL/g for CS2) with respect to the first two samples in Table III. Laboratory pulps with lower viscosity than the commercial ones were obtained at similar $kappa$ numbers. This behavior has been previously observed in our work group, and it could be attributed to the fact that laboratory-scale equipment is considerably smaller than industrial pulping reactors; the former has a higher metal-surface- to-pulp ratio than the latter. Therefore, there was a greater deterioration of the fiber in contact with the metal wall.

3.3. Paper properties

This section outlines the paper properties achieved with the different studied pulps. The pulps were refined at different revolutions, as indicated in Section 2. The different properties measured at each revolution are shown in the figures, as well as the trends observed. The notation used is as follows: AA14 (sawmill chip wood; alkali charge: 14 % as Na₂O; H-factor: 1260), AA16 (sawmill chip wood; alkali charge: 16 % as Na₂O; H-factor: 1080), FTW (final turn wood; alkali charge: 14 % as Na₂O; H-factor: 1080), TW (thinning wood; alkali charge: 14 % as Na₂O; H-factor: 1260), CS1 (commercial sample 1), CS2 (commercial sample 2).

3.3.1. Drainability

The drainability was quantified by measuring the CSF, as shown in Fig. 1.

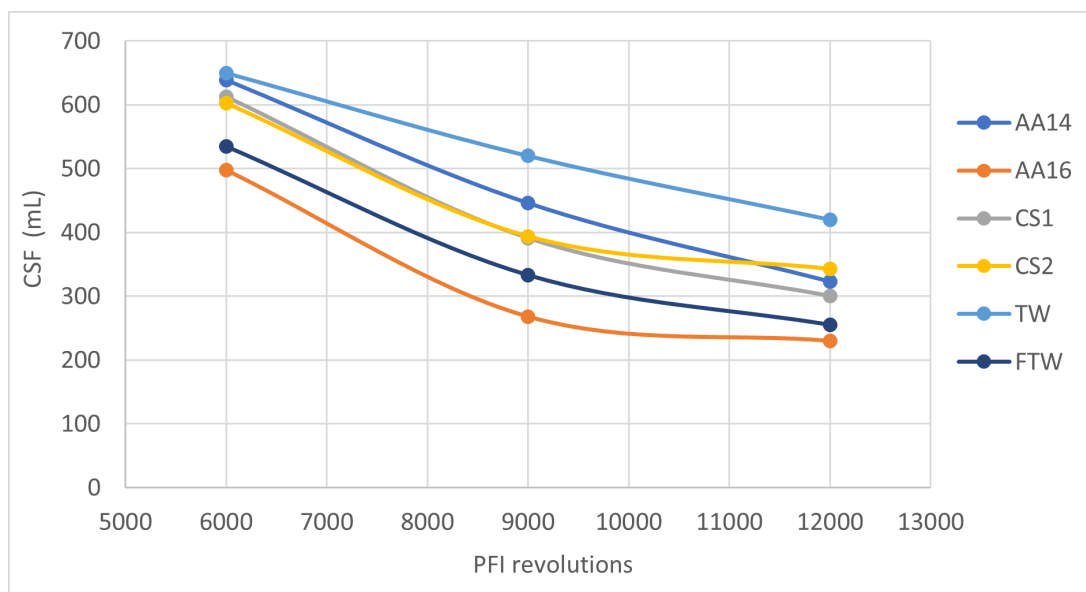


Figure 1. Drainability (mL) according to CSF measurements for four laboratory pulps and two commercial brown pulps

The results showed the expected trend: drainability values decreased when refining increased due to the fibrillation phenomenon (17). Sample AA14 exhibited the highest drainability values for all the revolutions tested. Thus, it was considered to be the fiber with the least damage.

3.3.2. Air permeability

Fig. 2 shows the air permeability values, which increased for all samples as the number of revolutions increased. The reason for this is that the higher the refinement, the greater the fibrillation. Therefore, the sheets produced with more refined pulps were more compact and less porous. When partitioning by sample, a statistically significant difference between the three refining points was found, except for the thinning sample, which reported no significant difference between 9000 and 12 000 revolutions. When partitioning by degree of refinement, it was observed that, at 9000 and 12 000

revolutions, sample AA14 was the least porous, which agreed with the previous result, exhibiting the lowest drainability values. This implies that sample AA14 is the most resistant fiber to mechanical treatment.

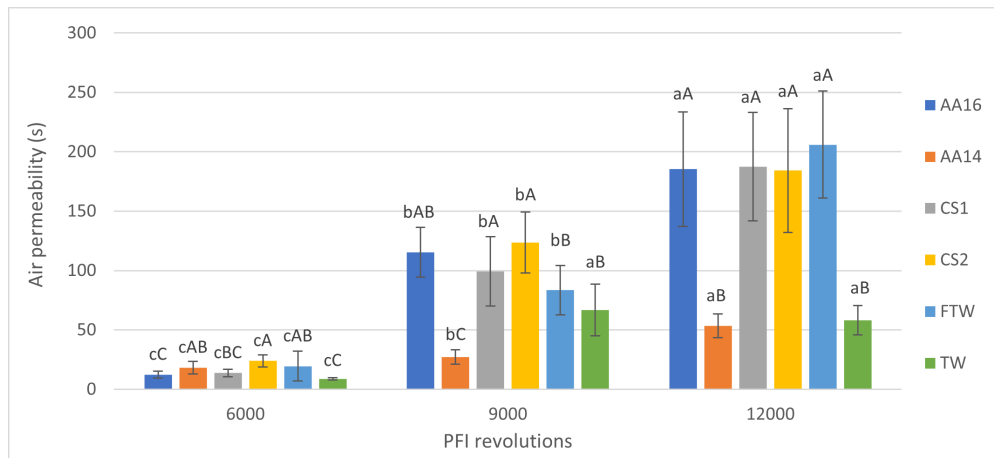


Figure 2. Air permeability (s) values for the sheets evaluated with the different samples at different PFI revolutions. Lowercase letters are used to compare different samples with the same PFI revolutions. Capital letters are used to compare the same pulp at different PFI revolutions. The same letter indicates no statistical differences between the samples.

3.3.3. Opacity

The opacity value (Fig. 3) decreased as the number of revolutions increased. This behavior was expected, as the sheets were more compact when the opacity decreased. This could be explained by the external fibrillation generated during the refinement of the pulp produced with a more closed framework, wherein fines were generated, filling the spaces between the fibers. When partitioning by samples, the statistical analysis showed statistically significant differences for samples AA14 and TW at 6000 revolutions, as well as for samples CS2 and FTW at 12 000 revolutions, for which no trend was evident.

3.3.4. Tear resistance index

According to the values presented in Fig. 4, the tear strength index value decreased as the number of revolutions increased, possibly due to the deterioration of the fiber due to mechanical action. At 6000 revolutions, samples AA14 and AA16 reported a higher tear strength index value. The same trend was maintained for the different degrees of refinement, meaning that these samples had the longest fiber length. This could be explained by the fact that samples AA14 and AA16 corresponded to the older specimens.

Except for sample AA14, no statistically significant difference was observed at 9000 and 12 000 revolutions when partitioning by sample; increasing the refining process did not cause perceptible damage to the analyzed pulps.

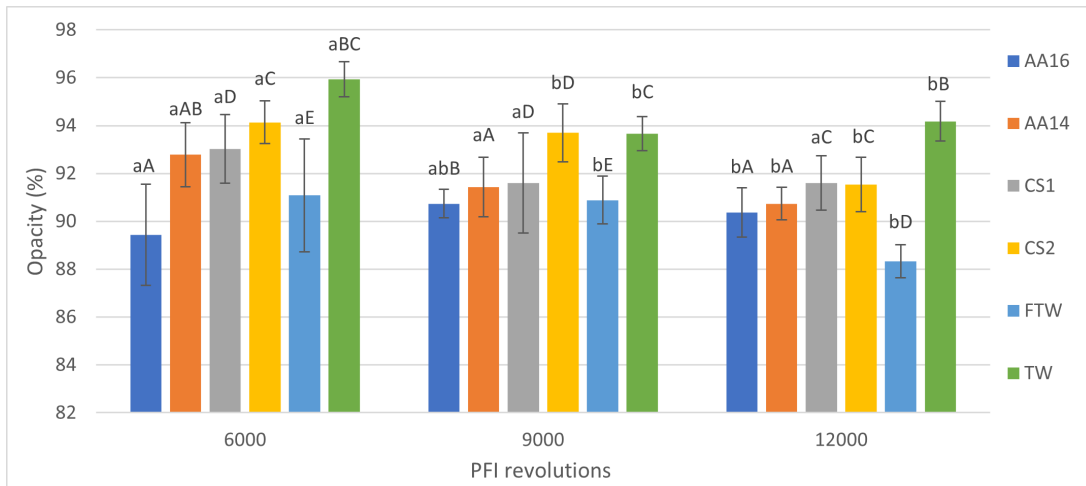


Figure 3. Opacity (%). Lowercase letters are used to compare different samples with the same PFI revolutions. Capital letters are used to compare the same pulp at different PFI revolutions. The same letter indicates no statistical differences between samples.

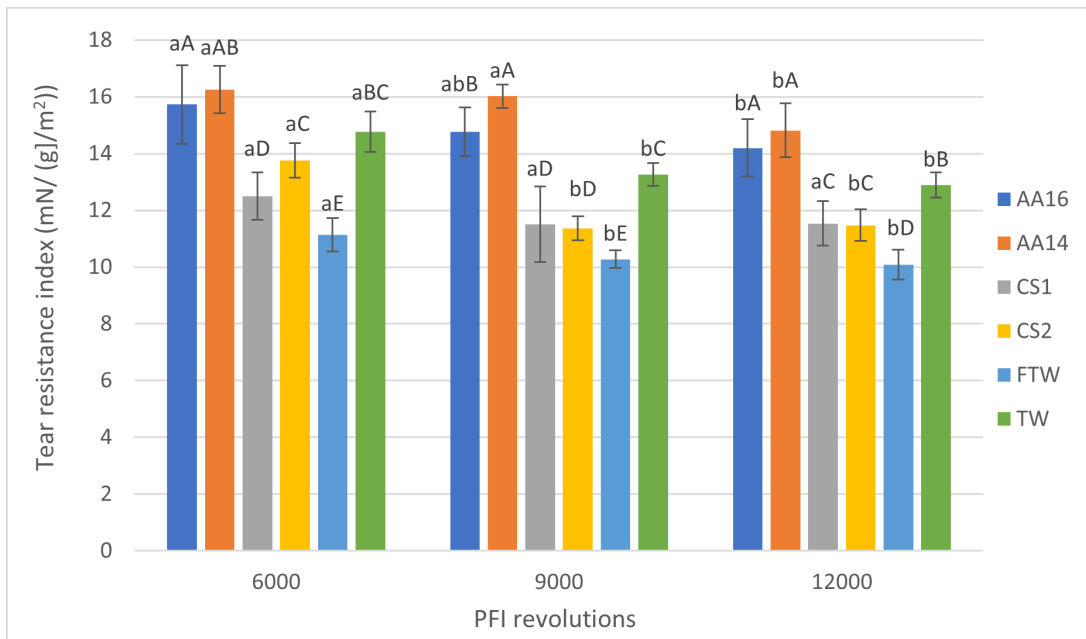


Figure 4. Tear resistance index (mN/[g/m²]). Lowercase letters are used to compare different samples with the same PFI revolutions. Capital letters are used to compare the same pulp at different PFI revolutions. The same letter indicates no statistical differences between samples.

3.3.5. Tensile strength index

Fig. 5 shows the tensile strength indices for different levels of refinement. These values increased with the number of revolutions because the external fibrillation phenomenon produced during refinement generates a greater number of resistant bonds (26). When partitioning by sample, a similar

behavior was observed in the opacity measures. Thus, the trend was not clear. When partitioning by degree of refinement, at 6000 revolutions, there was no statistically significant difference between the samples. However, for higher refinement revolutions, the samples were differentiated, with the final-turn pulp having the best response to the process.

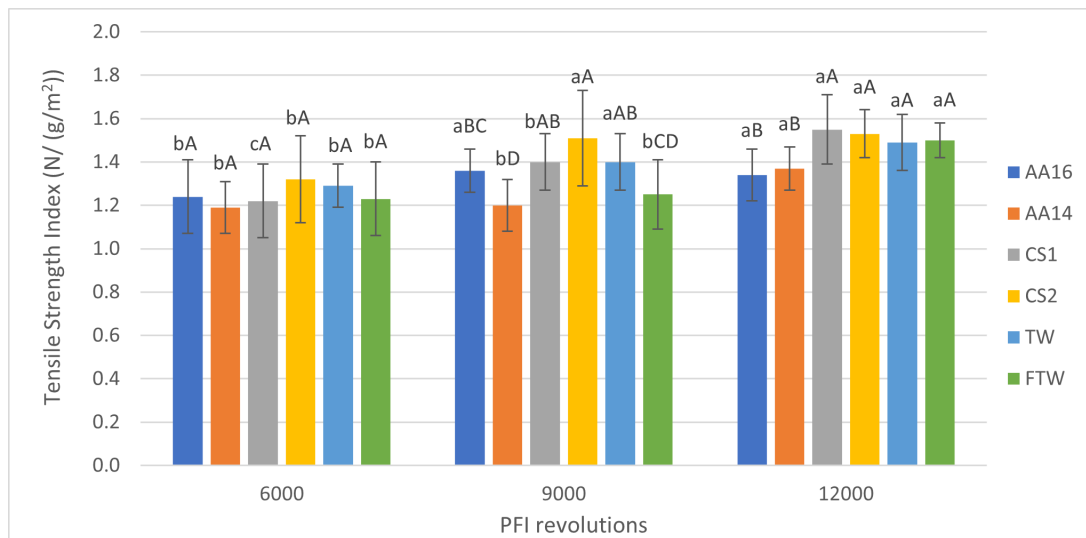


Figure 5. Tensile strength index (N/[g/m²]). Lowercase letters are used to compare different samples with the same PFI revolutions. Capital letters are used to compare the same pulp at different PFI revolutions. The same letter indicates no statistical differences between samples.

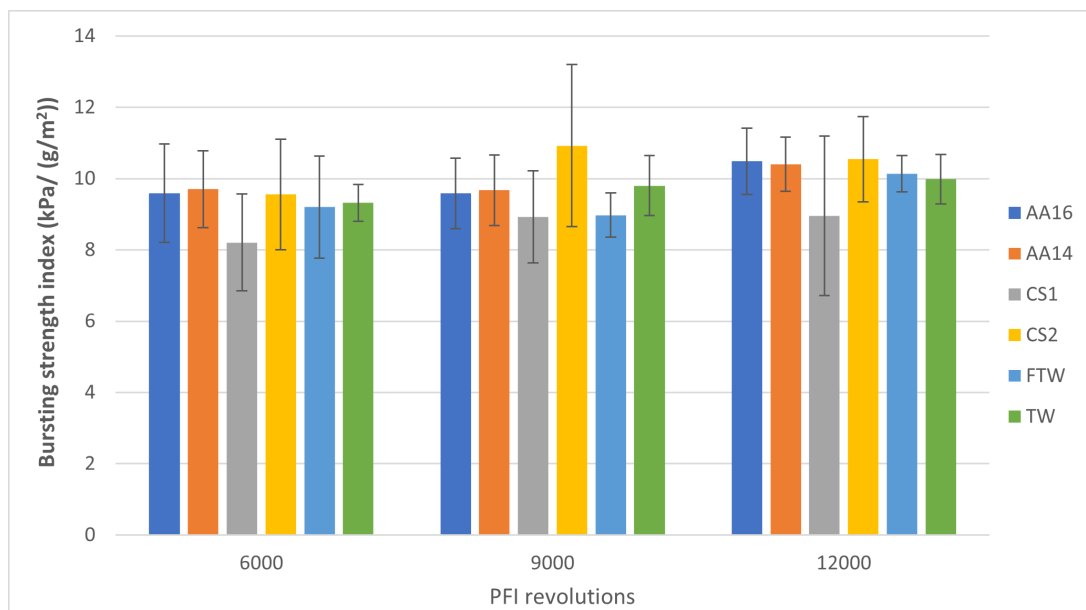


Figure 6. Bursting strength index (kPa/[g/m²]). Lowercase letters are used to compare different samples with the same PFI revolutions. Capital letters are used to compare the same pulp at different PFI revolutions. The same letter indicates no statistical differences between samples.

3.3.6. Bursting strength index

The values obtained for this index are shown in Fig 6. Although the distribution of errors of the experimental measurements did not allow for statistical analysis, the resistance values obtained with the experimental samples were similar to each other as well as to those obtained from commercial pulps. This measure is similar to that reported by other authors (27).

4. Conclusions

Based on the experimental data, sawmill by-product chips were found to be a viable raw material for use in a kraft pulp mill. Out of the sawmill chips used, 85 % had a suitable size for use as raw, while 11 % were larger and could be re-chipped.

The three types of wood tested exhibited similar chemical compositions and small differences in their basic density and lignin contents, which could be explained by the presence of branches in the composition of the composite mixture.

It was possible to obtain pulp with a *kappa* number of 80 under an active alkali charge of 14 % (Na₂O) and an H-factor of 1260 for sawmill chips and thinning wood, as well as 14 % (Na₂O) and an H-factor of 1080 for final-turn wood. These pulping conditions resembled those reported in the literature, in addition to the yields and the rejection values obtained. However, the viscosity values were lower than expected.

This difference could be explained by the differences between the methods used, as our measurements were outside the standard method conditions.

Sample AA14, which corresponds to sawmill chips pulped with a 14 % acetic alkali charge (Na₂O) and an H-factor of 1080, exhibited the best quality in terms of paper properties, with the highest CSF and tear index values. Likewise, the final-turn sample was shown to be the most sensitive to the refining process, reporting the lowest tear resistance indices and the most compact sheets.

In this vein, it can be stated that the brown kraft pulp produced with the *Pinus taeda* wood available in Uruguay exhibits adequate quality and can be marketed as an input to produce packaging paper.

The results obtained in this research confirm the technological feasibility to produce *Pinus taeda* brown kraft pulp mill. In the future, an economic and environment study could be conducted to determine the feasibility of installing an industrial-size mill in Uruguay.

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Viviana Palombo: Conceptualization, data curation, formal analysis, investigation, writing (original draft, review & editing).

Leonardo Clavijo: conceptualization, investigation, writing (review & editing).

Maria Noel Cabrera: conceptualization, investigation, writing (review & editing).

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